PATENT SPECIFICATION



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COMPLETE SPECIFICATION.

An Improved Method and Apparatus for Heating and Cooling Fluids.

We, LA GIRATION DES FLUIDES, a Body Corporate organised under the laws of the French Republic, of rue George Sand, Montluçon, Allier Department, France, 5 do hereby declare the nature of this invention and in what manner the same is to be performed, to be particularly described and ascertained in and by the following statement:-

The object of our invention is a method for automatically obtaining from a fluid under pressure a current of hot fluid and a current of cold fluid, that transformation of the initial fluid into two currents 15 of different temperatures taking place without the help of any movable mechanical element, merely through the work of the molecules of fluid upon one another.

The method according to this invention consists in causing fluid to flow with a gyratory helical motion along a surface of revolution, and in dividing the fluid into two coaxial sheets which move along 25 each other so that the outer sheet is compressed by the inner one and by the action of centrifugal force, whereby the work thus produced causes a rise in the temperature of the outer sheet and a fall in 30 the temperature of the inner sheet.

In a practical mode of carrying out this method, the fluid under pressure is introduced tangentially into a vessel hav-ing the shape of a body of revolution 35 provided with axial orifices disposed on either side of the fluid inlet. Said fluid is suitably guided so as to give it a helical motion toward one of said orifices, the cross section of which is suitably re-40 stricted so as to produce a backward motion of a portion of the fluid toward the opposite orifice. This produces two sheets of fluids having opposite axial motion the inner sheet expanding and 45 compressing the outer sheet thus supplying heat thereto. A current of hot fluid is thus received through the orifice of restricted cross section, while a current of [Price 1/-]

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cold fluid is received through the opposite orifice.

Another object of our invention is to provide an apparatus for carrying out the method above referred to. According to our invention, this apparatus comprises a chamber having the shape of a body of revolution the middle part of which is provided with one or more tangential inlet tubes for the fluid under pressure. Axial orifices are provided at either end of said chamber, one of said orifices, to-ward which the liquid, or fluid is directed through a suitable guiding with a gyratory motion, having a cross section smaller than that of the sheet of fluid, so that a portion of the latter is driven back toward the opposite orifice in such manner that it is caused to flow over the sheet of fluid that is applied against the wall of the chamber in question.

Preferred embodiments of our invention will be hereinafter described with reference to the accompanying drawings, given merely by way of example, and in which:

Figs. 1 to 5 inclusive are diagrammatical views illustrating the principle of our invention, Fig. 2 being a sectional view on the line 2—2 of Fig. 1.

Fig. 6 is a diagrammatical view of an embodiment of our invention.

Fig. 6^a is a sectional view on the line 6^a-6^a of Fig. 6.

Fig. 7 is a detailed view showing in

axial section a practical embodiment of our invention.

Fig. 8 is a corresponding plan view at a smaller scale.

Fig. 9 is a diagrammatical elevational view of another embodiment of our invention.

Fig. 10 is an end view corresponding

Fig. 11 is a diagrammatical view of another embodiment of our invention.

Fig. 12 is an end view corresponding to Fig. 11.

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Figs. 13 and 14 are diagrammatical views of two other embodiments of our

invention.

The principle on which our invention 5 is based is illustrated by diagrammatic figures 1 to 5. Supposing as shown in Figs. 1 and 2, that a tube A B is provided in its middle part with a tangential inlet pipe 1 through which a current 10 of fluid under pressure is sent into said tube, said fluid is given in said tube a certain linear velocity parallel with the axis of said tube, said rectilinear movement being combined with a gyratory 15 movement about the axis of the tube. The fluid flows toward both ends of the

As the fluid is moving away from the inlet pipe, its rectilinear velocity, which 20 is parallel with the axis x y of the tube, increases and its angular velocity creases, so that the fluid spreads along the wall of the tube so as to form a sheet 2 having substantially the shape of a body of revolution about axis x y (Fig. 3). In said sheet the molecules are subjected to a pressure which is the higher as they are at a greater distance from the axis of the tube due to the action of the 30 centrifugal force. At the same time, the flow of the fluid produces a substantial fall of pressure in the central zone of the tube, so that the outer air, which is at the atmospheric pressure, is drawn to-ward the central zone of the tube, thus forming two axial currents 2ⁿ (Fig. 4). When the outer air reaches said central zone, it is driven back toward the outside by the fluid moving with a gyratory 40 movement thus forming streams 3.

If an annular diaphragm 4, the free central opening 4^a of which has a diameter equal to the minimum diameter of the zone in which a fall of pressure is 45 produced, as shown in Fig. 5, is provided in the central part of the tube, on one side of the tangential inlet pipe, the fluid moving with a gyratory movement will flow only toward orifice B, carrying along with it the atmospheric air coming from both orifice A and orifice B.

The method and the apparatus according to our invention are based on the experimental facts that have just been

In the embodiment shown in Figs. 6 and 6°, the apparatus consists chamber 5, having the shape of a body of revolution about axis x y, the middle 60 part 6 of said chamber being of restricted cross section and being provided with a tangential inlet pipe 7 for the fluid under The inner wall of chamber is provided, opposite the opening of said 65 pipe, with a helical guiding surface 8.

The orifice A of chamber 5 is freely opened, while the cross section of orifice B is restricted by a kind of frustoconical diaphragm or deflector 9, so that the fluid under pressure, admitted through pipe 7, is only allowed to flow through an annular aperture 10, which is not sufficient for the amount of fluid fed thereto. The fluid under pressure, admitted through pipe 7 and guided by helical surface 8 is simultaneously given a rectilinear motion which causes it to move within chamber 6 toward opening 10, and a rotary motion about axis x y. The sheet of fluid that is immediately adjacent the wall of the chamber flows out through said opening 10, while the remainder of the fluid, which is prevented from flowing out by diaphragm 9 is subjected to the fall of pressure existing in the central zone of the chamber and is given a backward motion toward orifice A. We thus obtain, according to our invention, a first sheet of fluid 11, moving with a gyratory motion along the inner wall of the chamber, from orifice 7 toward orifice B, and a second sheet of fluid 12 moving with a gyratory motion along the inner surface of the first mentioned sheet in an opposite axial direction, said second sheet of fluid consisting of the difference between the amount of fluid admitted through pipe 7 and the amount of fluid that is allowed to flow out through Said sheet of fluid under 100 opening 10. pressure 12, which moves with a gyratory motion not along the rigid wall of chamber 5, but along the elastic surface of the first mentioned sheet of fluid, tends on the one hand under the action of the cen- 105 trifugal force, and on the other hand under the effect of the increase of velocity due to the expansion and to the rotation that take place, to compress the molecules of the first mentioned sheet of fluid. 110 compression absorbs a certain amount of work, which is evidenced by a loss of heat from the second mentioned sheet to the benefit of the first mentioned one. Consequently, the temperature of 115 sheet 12 falls, while the temperature of Finally, there is obtained sheet 11 rises. through orifice 10 a current of hot fluid and through orifice A a current of cold

The initial guiding of the fluid toward one of the orifices is necessary for practical purposes in order to obtain an accurate centering of the central zone of depression or fall of temperature. In 125 the example above described, that guiding is effected through helical inclined surface 8. The following description will show that the same result could be obtained through other guiding means.

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The adjustment of the cross section of the outlet orifice at B, which can be obtained through any suitable means makes it possible, by modifying the rates of flow at B and A, to vary the difference between the temperature of the initial fluid and those of the hot fluid and of the cold fluid escaping through outlet orifices B and A respectively.

If, for instance, the cross section of

the orifice 10 through which the hot fluid is allowed to flow out is considerably restricted, the rate of flow of the hot fluid is diminished, but the rate of flow of the 15 cold fluid is simultaneously increased so that the heat that is given out from one sheet to the other one causes a considerable rise of the temperature of the hot fluid but a small fall of the tempera-20 ture of the cold fluid, as compared with

that of the initial fluid. Fig. 7 shows a practical embodiment

of our invention.

This embodiment comprises a cylin-25 drical chamber 12 in which the inter-change of heat takes place, and an annular distributing organ made of two pieces 13-13a which is provided with an inlet pipe 14 for the fluid under pressure. Said distributing organ comprises an inner cylindrical chamber 15 connected with cylinder 12 through a frusto-conical surface 16, and with annular conduit 17 of the distributing annuar conduit 17 of the distributing organ through a tangential passage 17^a. The guiding helical surface 8 extends from one edge to the other of the orifice of said passage. The tangential passage 17^a and the guiding inclined surface 8 are provided in a separate part 19, provided with conical surfaces for the centering thereof between parts 13 and centering thereof between parts 13 and 13° of the distributing organ. On the side opposite to cylinder 12 said distri-45 buting organ is connected with a cylinder 21 at the end of which the current of cold fluid is received, while the current of hot fluid passing through the annular orifice provided around conical dia-phragm 9 is received through tube 22.

Figs. 9 to 13 show other embodiments of the means for guiding the fluid. In the embodiment of Figs. 9 and 10, said guiding is obtained through several tan-55 gential pipes 7^a opening into a frusto-conical chamber 23 connected with the

working chamber 12.

In the embodiment of Figs. 11 and 12, the guiding action is obtained through 60 several pipes 7° opening tangentially into chamber 12, but which are inclined with

respect to the axis x y of said chamber. Furthermore, instead of being provided on either side of the inlet conduit, the 65 axial orifices through which the two sheets

of liquid escape may be disposed on the same side of said inlet conduit, annular orifice for the outflow of the hot fluid surrounding the outlet orifice for the cold fluid. In such an arrangement, the two sheets have parallel axial movements in the same direction, which may be advantageous in some cases for reduc-ing their mutual friction.

Such an arrangement is shown in Fig.

13 in which the fluid is admitted at one of the ends A of the chamber A B having the shape of a body of revolution and is given a gyratory movement by a plurality of blades 23 disposed in an annular The other end B of chamber tube 24. A B is provided with two concentric orifices 10 and 25 disposed in such manner that the outer orifice is limited by a diaphragm 9 so that the fluid moving with a gyratory motion from end A past blades 23 cannot escape entirely through said orifice 10. A part of said fluid is compelled to escape through the inner orifice 25, of smaller diameter, which

corresponds to a zone of lesser pressure.

This causes an expansion of that portion of the fluid and it has been ascertained experimentally that said expansion starts as soon as the fluid leaves the directing blades and is continued as far as orifice 25. According to the laws of gyratory flow, said expanding sheet compresses the sheet that surrounds it and that flows out through annular orifice 10 100 and tube 26. In order to avoid parasitic entrainments, it is advantageous to give also to orifice 25, an annular shape by means of a deflector 27, along which the inner sheet flows before reaching tube 28. 105 To sum up, tube 28 serves to the outflow of a portion of the fluid that is cooled by expansion with production of external work and tube 26 serves to the outflow of the remaining portion of the fluid, 110 which is heated by compression.

Finally, instead of extracting the initial energy that is necessary for the working of the apparatus from a compressed air reservoir, it may be necessary 115 in some cases to make use of mechanical energy for imparting a gyratory movement to the fluid and for giving it the super-pressure that is necessary for its flow through the apparatus. To this 120 effect, we may dispose, in concentric relation with the stationary blades that control the inlet of fluid, a plurality of movable blades which are mechanically actuated and are disposed in the same 125 manner as the rotor of an air fan or of

a compressor.

Such an arrangement is diagrammatically shown in Fig. 14 in which the initial energy of the fluid is not due to a pre- 136

liminary compression in a separate apparatus but is imparted thereto in the apparatus itself by means of a rotor with blades 29 which is mechanically 5 driven by a shaft 30.

The means for introducing the fluid under pressure into the chamber of revolution may be a fan disposed opposite the inlet end of the chamber and externally

10 thereof.

In this embodiment all the other parts are disposed in the same manner as in the apparatus of Fig. 13, with the exception of deflector 27 which is replaced by an annular body 31 extending along the whole length of chamber A B, which is preferable when the diameter of the latter is relatively large.
While we have described what we deem

20 to be preferred embodiments of our invention, it should be well understood that we do not wish to be limited thereto as there might be changes made in the arrangement, disposition and form of the parts 25 without departing from the principle of

our invention.

It will be understood that it is advantageous to reduce the interchanges of heat between the various parts and between 30 said parts and the outside by means of suitable heat insulating arrangements. Finally the adjustment of the difference of temperature between the hot sheet of fluid and the cold sheet may be obtained by modifying the ratio of the flows of the hot and cold fluids to the initial flow, which may be produced by modifying the sections or the inlet or outlet pressure of one of the three currents of fluid. 40 particular, in order to increase the temperature of the hot sheet, we may restrict the section left by diaphragm 9 for the outlet of said sheet or reduce the rate of flow by means of a valve disposed on the outlet pipe for the outflow of the heat fluid, or increase the initial pressure of the fluid admitted into the apparatus or again act on the section or the pressure at the outlet of the cold sheet.

Having now particularly described and ascertained the nature of our said invention and in what manner the same is to be performed, we declare that what we

claim is:

1. A method of obtaining from a current of fluid under pressure a current of hot fluid and a current of cold fluid which method comprises causing said fluid to flow with a gyratory helical motion along a surface of revolution, and dividing said fluid into two coaxial sheets moving along each other so that the outer sheet is compressed by the inner sheet and by the action of centrifugal force, whereby

the temperature of the outer sheet and a fall in the temperature of the inner sheet.

2. Apparatus when used for obtaining a flow of hot fluid and a flow of cold fluid from a current of fluid under pressure, which apparatus comprises in combination, a chamber having the form of a body of revolution, means for introducing fluid under pressure into this chamber and of imparting to it in the said chamber a gyratory movement, annular orifice of relatively large diameter being provided in the walls of the said chamber to receive the hot fluid, and a second orifice, of relatively smaller diameter than the first, being adapted to receive a current of cold fluid. the chamber having in its interior no mechanical element, the hot fluid escaping through $_{
m the}$ larger orifice and cold fluid escaping through the smaller orifice, two concentric layers in contact with one another being formed in the interior

3. An apparatus according to Claim 2, in which the chamber having the shape of a body of revolution is provided with axial orifices at either end and comprises means for introducing the fluid under pressure tangentially into the middle part of said chamber, means for helically guiding said fluid toward one of said orifices and means for partly stopping the last-mentioned orifice so as to leave only an annular passage for the outflow of the fluid, the other orifice being open to the atmosphere.

4. An apparatus according to Claim 3, in which the last-mentioned means are adjustable so as to make it possible to vary the cross section of the annular passage for the fluid.

5. An apparatus according to Claim 2, 110 which comprises in combination, a chamber having the shape of a body of revolu-tion provided with axial orifices at either end, at least one tangential inlet pipe for the fluid under pressure opening into the 115 middle part of said chamber, means for helically guiding said fluid from said pipe toward one of said orifices and a deflector for partly stopping the last mentioned orifice so as to leave only an annular outlet passage for the fluid, the other orifice being open to the atmosphere.

6. An apparatus according to Claim 3 in which the means for guiding the fluid consist of a member having a helically inclined surface located opposite the opening of said inlet pipe into said chamber.

7. An apparatus according to Claim 3 65 the work thus produced causes a rise in in which the means for guiding the fluid 130

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under pressure consist of a frusto-conical chamber coaxially connected with the first mentioned chamber, the apparatus comprising a plurality of fluid inlet pipes 5 tangentially connected with said frustoconical chamber.

8. An apparatus according to Claim 2 which comprises in combination, a chamber having the shape of a solid of revolu-10 tion provided with an axial orifice at either end, a plurality of tangential inlet pipes for the fluid under pressure opening into said chamber, said pipes being inclined with respect to the axis of said chamber 15 so as to guide the fluid toward one of said orifices, and a deflector for partly stopping the last mentioned orifice so as to leave only an annular outlet passage for the fluid, the other orifice being open 20 to the atmosphere.

9. An apparatus according to Claim 3 in which the chamber has a restricted cross section between the opening of the inlet pipe and the last mentioned orifice.

10. An apparatus according to Claim 3 in which there is provided a distributing organ made of two parts located opposite said inlet pipe, the guiding means consisting of a ring provided with a tan-30 gential inlet conduit and with an inclined helical surface, which ring is inserted between said two parts of the distributing

11. An apparatus according to Claim 2, 35 which comprises in combination, a chamber having the shape of a surface of revolution, an inlet pipe for introducing fluid into said chamber, a plurality of directing blades located opposite said pipe 40 for imparting to said fluid a gyratory motion along the inner wall of said chamber and means for dividing said fluid

into two concentric sheets so that one of said sheets gives up a portion of its heat to the other sheet.

12. Apparatus according to Claim 2, in which the outlet orifices for the hot and the cold fluid are of annular form and are arranged at the same end of the chamber of revolution.

13. An apparatus according to Claims 2, 11 and 12, in which an inlet pipe for introducing fluid under pressure into the chamber of revolution is disposed coaxially with said chamber at one end thereof, a plurality of directing blades in said chamber are disposed opposite said inlet pipe for imparting to said fluid a gyratory motion along the inner wall of said chamber, and two annular orifices are disposed at the opposite end of said chamber coaxially therewith for dividing said fluid into two concentric sheets one of which gives up a portion of heat to the other one.

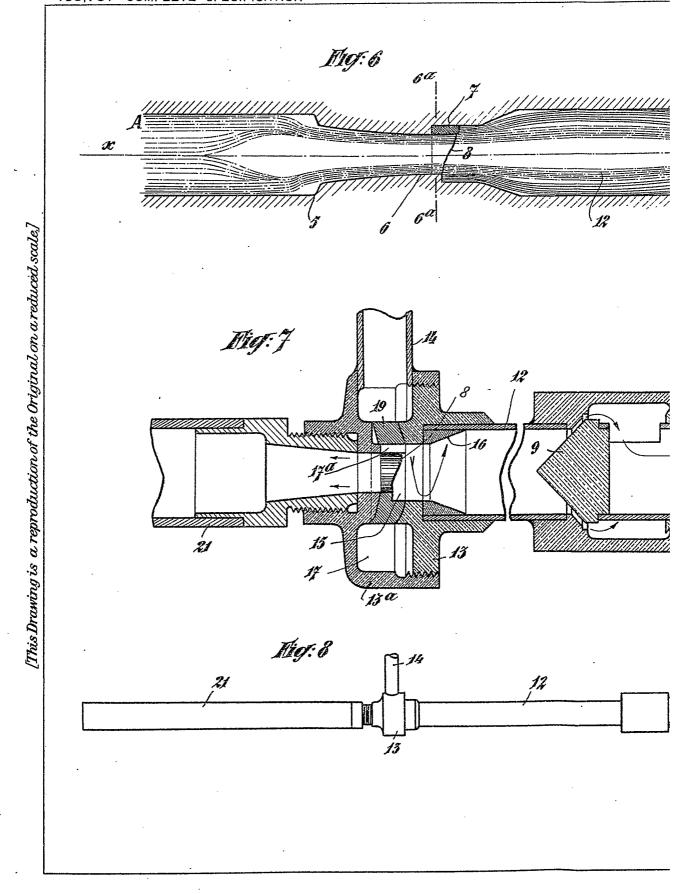
14. Apparatus according to Claim 12, in which the means serving to introduce the fluid under pressure into the chamber revolution are mechanical means arranged externally of the said chamber and combined with directing means which serve to impart to the fluid a gyratory movement in the interior of the chamber

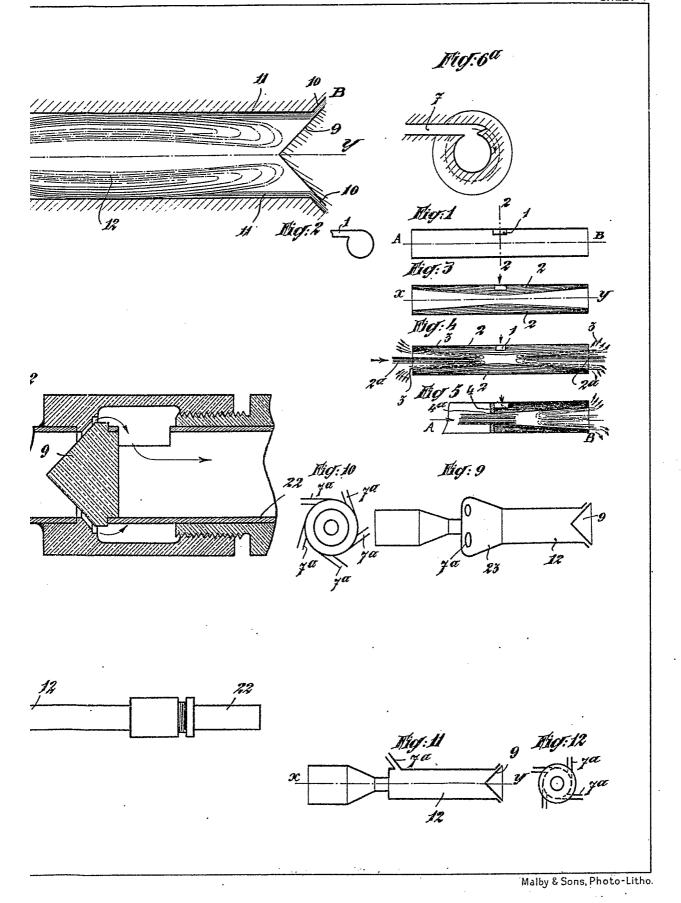
of revolution.

15. An apparatus according to Claim 14, in which the mechanical means consist of a fan disposed opposite the inlet end of said chamber.

Dated this 12th day of December, 1932. ABEL & IMRAY, Agents for the Applicants, 30, Southampton Buildings, London, W.C. 2.

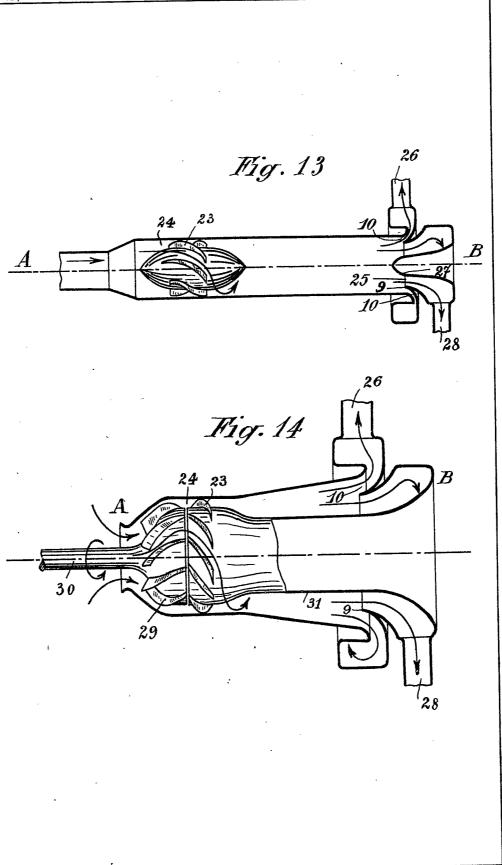
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